

**LISTING OF CLAIMS IN THE APPLICATION**

1 (currently amended). A catalyst complex for esterification and trans-esterification reactions, comprising:

i) a polymeric titanium glycolate represented by the formula  $[TiO_4(CH_2)_4]_n$  wherein  $n = \underline{\text{up to } 200}$ ; and

ii) an alkali metal glycolate,

wherein the molar ratio of the polymeric titanium glycolate and the alkali metal glycolate is ~~about 1.25:1~~ to ~~about 100:1~~.

2. (previously amended) The catalyst complex according to claim 1, wherein the alkali metal glycolate is represented by the formula  $Na-O-CH_2-CH_2-OH$ .

3. (currently amended) The catalyst complex according to claim 1, wherein the molar ratio of the polymeric titanium glycolate and the alkali metal glycolate is ~~about 1.25:1~~ to ~~about 10:1~~.

4. (previously amended) A process for the esterification of a dicarboxylic acid compound and an alcohol compound comprising contacting a process feed comprising a dicarboxylic acid compound and an alcohol compound with the catalyst complex of claim 1, wherein the dicarboxylic acid compound is represented by the formula  $HOOC-R-COOH$ , wherein R is a linear or branched alkyl, alkenyl or aryl group containing 2 to 30 carbon atoms.

5. (previously amended) The process according to claim 4, wherein R contains 4 to 15 carbon atoms.

6. (previously amended) The process according to claim 5, wherein the dicarboxylic acid compound is selected from the group consisting of terephthalic acid, isophthalic acid, naphthalenic diacid, succinic acid, adipic acid, phthalic acid, glutaric acid, oxalic acid and maleic acid.

7. (previously amended) The process according to claim 6, wherein the dicarboxylic acid compound is terephthalic acid.

8. (previously amended) The process according to claim 4, wherein the dicarboxylic acid compound is an oligomer having repeating units derived from a carboxylic acid.

9. (previously amended) The process according to claim 4, wherein the alcohol compound comprises an alkylene glycol represented by the formula HO-R'-OH or a polyalkylene glycol represented by the formula HO-[R"-O-]<sub>n</sub>-H, wherein R' is a linear or branched alkyl group, having 2 to 10 carbon atoms, and wherein R" is an alkyl group having 1 to 10 carbon atoms.

10. (previously amended) The process according to claim 6, wherein the alcohol compound is selected from the group consisting of ethylene glycol, propylene glycol, isopropylene glycol, butylene glycol, 1-methyl propylene glycol, pentylene glycol, neopentylene glycol, and combinations thereof.

11. (previously amended) The process according to claim 4, wherein the process is carried out at a temperature of 150°C to about 500°C and at a pressure of about 0.001 atmosphere to about 10 atmospheres.

12. (previously amended) The process according to claim 10, wherein the process is carried out at a temperature of about 250°C to about 300°C and a pressure of about 0.001 atmospheres to about 10 atmospheres.

13. (previously amended) The process according to claim 4, wherein the molar ratio of the alcohol compound to the dicarboxylic acid compound is in the range of about 0.1:1 to about 10:1.

14. (previously amended) The process according to claim 10, wherein the catalyst complex is present in a concentration of about 1 ppm to about 70 ppm in the process feed.

15. (canceled).

16 (currently amended). The catalyst complex of claim 3, wherein the alkali metal glycolate glycolate is represented by the formula Na-O-CH<sub>2</sub>-CH<sub>2</sub>-OH.

17. (previously presented) The process according to claim 7, wherein the alcohol compound comprises ethylene glycol.

18. (previously presented) The process according to claim 10, wherein the molar ratio of the alcohol compound to the dicarboxylic compound in the process feed is in the range of about 1:1 to about 3:1.

19. (previously presented) The process according to claim 4, wherein the catalyst complex is present in a concentration of about 1 ppm to about 50 ppm in the process feed.

20. (previously presented) The process according to claim 9, wherein the catalyst complex is present in a concentration of about 1 ppm to about 50 ppm in the process feed.

21. (previously presented) The process according to claim 12, wherein the catalyst complex is present in a concentration of about 1 ppm to about 50 ppm in the process feed.